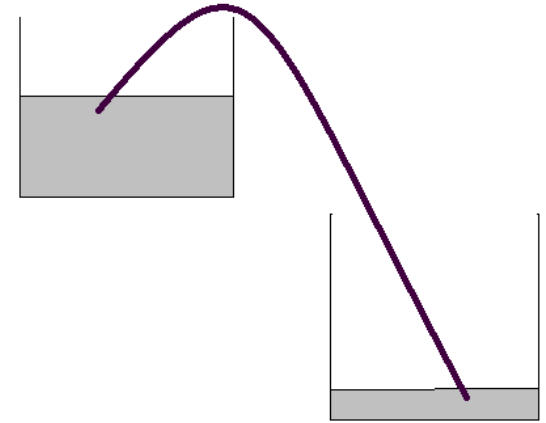


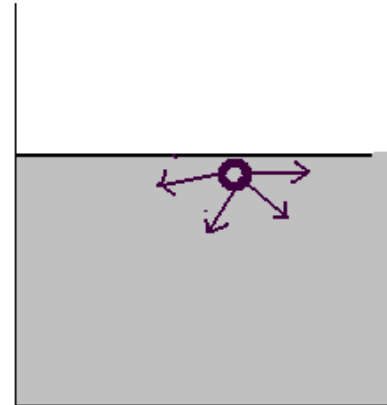
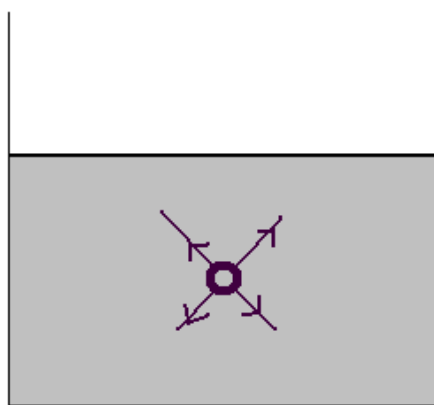
3.4. Surface tension and capillarity

From experiment: liquid thread, molecules of the liquid show cohesion.



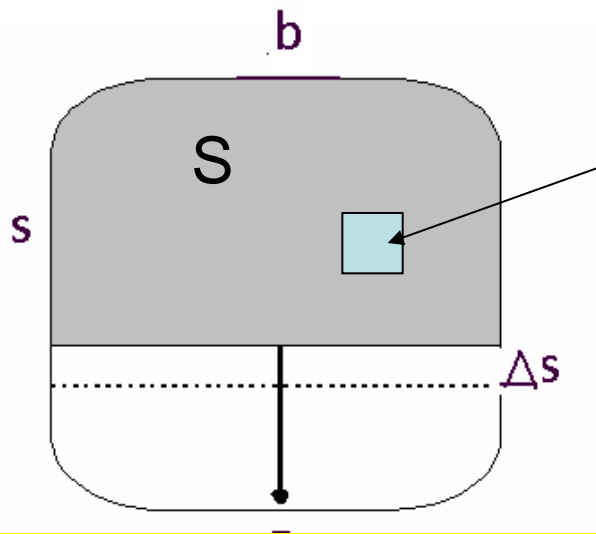
Properties of condensed matter:
Between molecules dominate
strong forces of short distances, 10^{-7}cm
practically up to the next neighbors.

Inside of the liquid: The forces cancel each other



On the surface:
It exists a resultant force towards inside.

At an increase surface: Against the forces ,
which pull towards inside, work ΔW has to be provided.



Referring to unit of area
 ΔS , a surface tension
will be defined:

a surface tension

$$\sigma_S = \frac{\Delta W}{\Delta S} \text{ with } \sigma_S \text{ (N/m)}$$

related to a unit surface unity

Example: Lamella of soap

Surface: $S=2 \cdot s \cdot b$

By a shift of the holder:

$$\Delta S = 2 \cdot b \cdot \Delta s \text{ with increase of energy:} \quad = \sigma_S = 2b \cdot \Delta s$$

$$\Delta W = \sigma_S \cdot \Delta S = \sigma_s \cdot 2b \cdot \Delta s \quad \text{Work done}$$

$$\Delta W = F \cdot \Delta s \quad \text{and thus} \quad \sigma_s = \frac{F}{2b}$$

$$\sigma_S = \frac{\Delta W}{\Delta S} \text{ with } [\sigma_S] = \frac{N}{m}$$

Example: Lamella of soap

$$\text{Surface: } S = 2 \cdot s \cdot b$$

Work done:

$$\Delta W = F \cdot \Delta s \text{ and thus } \sigma_S = \frac{F}{2b}$$

Surfaces of liquids are , minimal surfaces
i.e. at a given volume, lowest
surface

With increase of energy

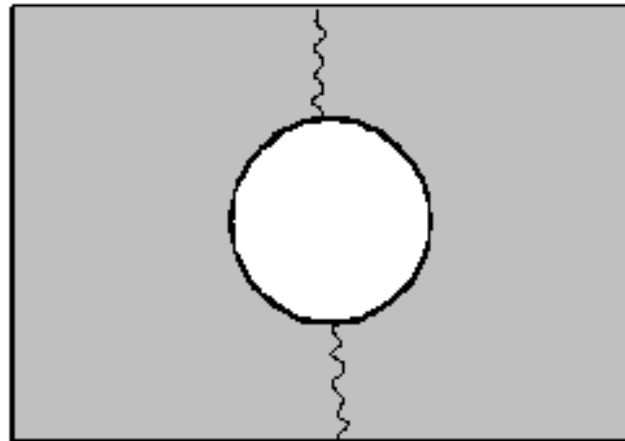
$$\Delta W = \sigma_S \cdot 2b \cdot \Delta s$$

For **water** one has:

$$\sigma_S = 0.073 N/m$$

For **mercury**:

$$\sigma_S = 0.47 N/m$$



Compression ratios in a soap bubble

Surface energy:

$$W_S = 2 \cdot \sigma_S \cdot 4 \cdot \pi \cdot r^2 = 8 \cdot \pi \cdot \sigma_S \cdot r^2$$

Smaller surfaces mean

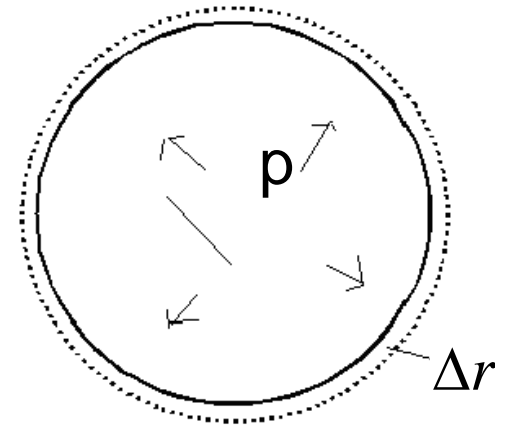
A win of energy!

$$\Delta W_S = 16 \cdot \pi \cdot \sigma_S \cdot r \cdot \Delta r > \text{Increase of pressure inside}$$

$$\text{Work done: } \Delta W_P = F \cdot \Delta r = p \cdot S \cdot \Delta r$$

$$\text{Being in balance: } \Delta W_S = \Delta W_P$$

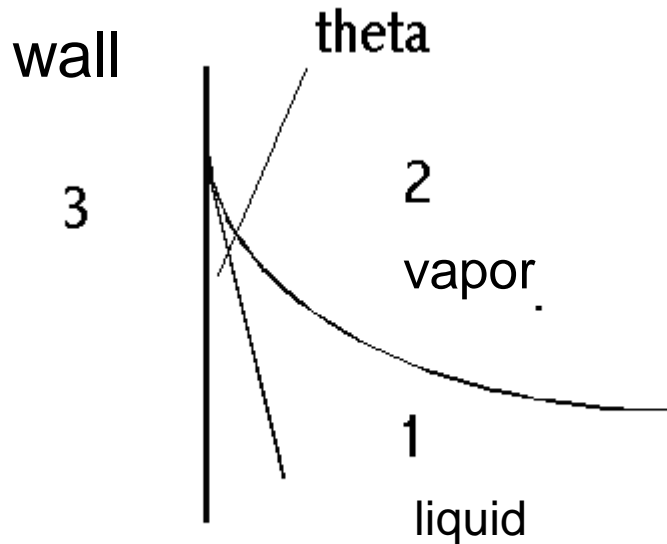
$$p = 4 \cdot \sigma_S / r$$



bubble smaller, pressure inside larger

Boundary surfaces: Up until now: Liquid - Gas

There are also boundary surfaces liquid-
liquid, liquid - all solid



Win of enrgy by coating of
boundary surfaces

Balance:

$$\underbrace{\sigma_{23} - \sigma_{12}}_{\text{adhesive tension: } \sigma_H} = \sigma_{12} \cdot \cos \theta$$

No balance : $\sigma_H \succ \sigma_{12}$:

**the liquid
crawls up the wall**

$0 \leq \sigma_H \leq \sigma_{12}$: coating "hydrophil"

$\sigma_H < 0$: no coating "hydrophob"

Capillarity:

Energy gain by wetting
of a surface of a cylinder

$$\Delta W_H = \sigma_H \cdot 2\pi \cdot r \cdot \Delta h$$

The work at lifting:

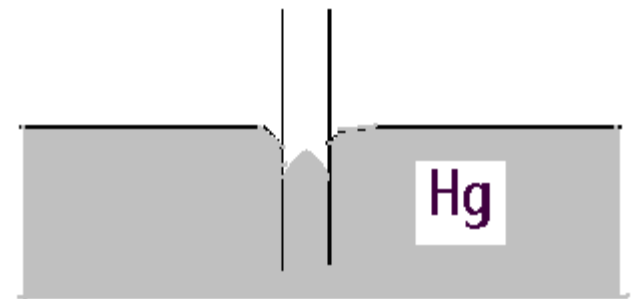
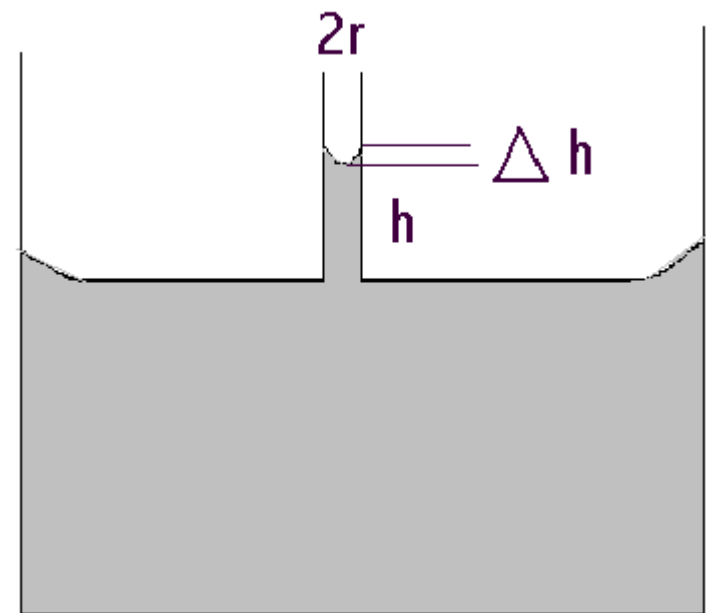
$$\Delta W_g = m \cdot g \cdot \Delta h$$

$$= \rho \cdot V \cdot g \cdot \Delta h = \rho \cdot g \cdot \Delta h \cdot \pi \cdot r^2 \cdot h$$

$$\text{balance} : \Delta W_H = \Delta W_g$$

Capillarity height:

$$h = 2 \cdot \sigma_H / \rho \cdot g \cdot r$$



3.5. Movements of liquids and gases

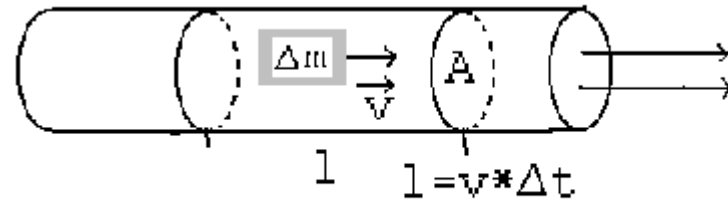
Uniform treatment of gases and liquids:

Velocity \ll Velocity of sound: common term:
Fluid. Three kinds of currents

- a) *Ideal liquid*: No forces of friction
- b) *Viscous flow*: Friction dominates
- c) *Turbulent flow* of real liquids

a)

Transport of liquids:



Flux:

$$\Phi = \frac{\text{mass of liquid entering through A in } \Delta t}{\text{time interval}}$$

$$\Phi = \frac{m(A, \Delta t, v)}{\Delta t} = \frac{\rho \cdot V(A, \Delta t, v)}{\Delta t} = \frac{\rho \cdot A \cdot v \cdot \Delta t}{\Delta t} = \rho \cdot A \cdot v$$

v : Not necessarily constant

$$\vec{j} = \rho \cdot \vec{v}$$

Density of current: Flux/Area

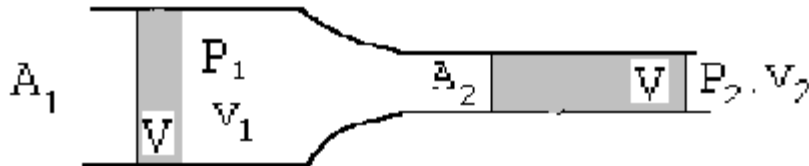
Principle of continuity: Flux remains preserved:

$$\Phi = \text{constant}$$



$$\Phi_1 = \Phi_2$$

$$\Rightarrow A_1 \cdot v_1 = A_2 \cdot v_2 \Rightarrow \frac{v_1}{v_2} = \frac{A_2}{A_1}$$



Volume of liquid wins
kinetic energy :

$$\Delta W_{kin} = \frac{1}{2} m v_2^2 - \frac{1}{2} m v_1^2 = \frac{1}{2} \rho \cdot V \cdot (v_2^2 - v_1^2)$$

In return **work** needs to be done!

V gets pressed into a pipe

$$\rightarrow T \approx \frac{R}{v}$$

$$\rightarrow P_2 \cdot V$$

$$v_1 < v_2 \Rightarrow \Delta W = P_1 \cdot V - P_2 \cdot V = (P_1 - P_2) \cdot V$$

$$\Delta W = P_1 \cdot V - P_2 \cdot V = (P_1 - P_2) \cdot V$$

Law of conservation of energy:

$$\Delta W = \Delta W_{kin}$$

$$P_1 \cdot V + \frac{1}{2} \rho \cdot V \cdot v_1^2 = P_2 \cdot V + \frac{1}{2} \rho \cdot V \cdot v_2^2$$

$$\Rightarrow P_1 + \frac{1}{2} \rho \cdot v_1^2 = P_2 + \frac{1}{2} \rho \cdot v_2^2$$

Is valid along of a arbitrarily formed pipe:

$$p + \frac{1}{2} \rho \cdot v^2 = \text{constant} = P_0$$

Equation of Bernoulli :

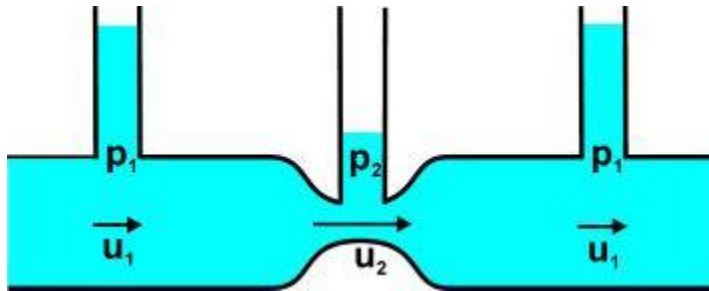
Static pressure+dynamic pressure=total pressure

Huge practical importance

$$v \sim \frac{1}{A} \Rightarrow$$

Static pressure large, if A large, dynamic pressure large, if A small

Hydrodynamic Paradoxon

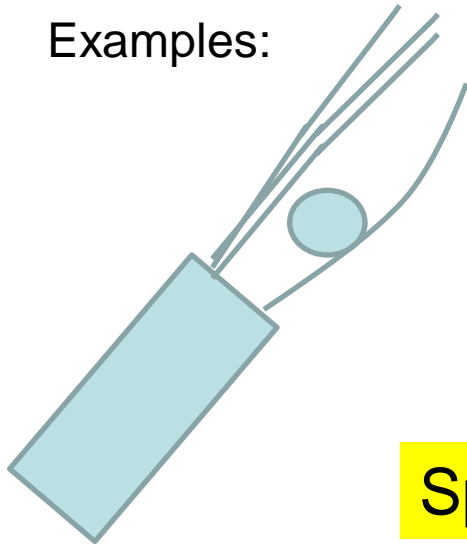


Accordingly:

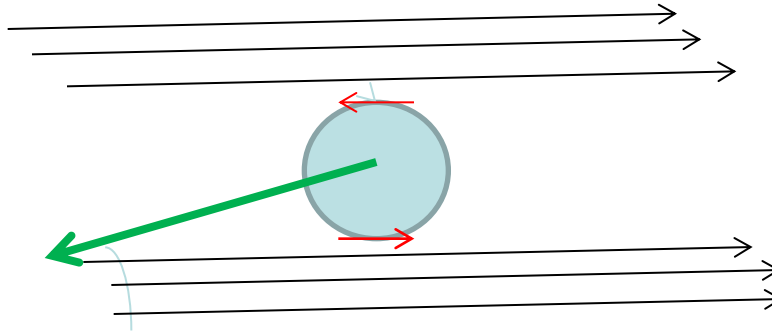
$$p + \frac{1}{2} \rho \cdot v^2 = P_0$$

„small“, if v large

Examples:



Magnuseffect



Sport: Ball „bending“

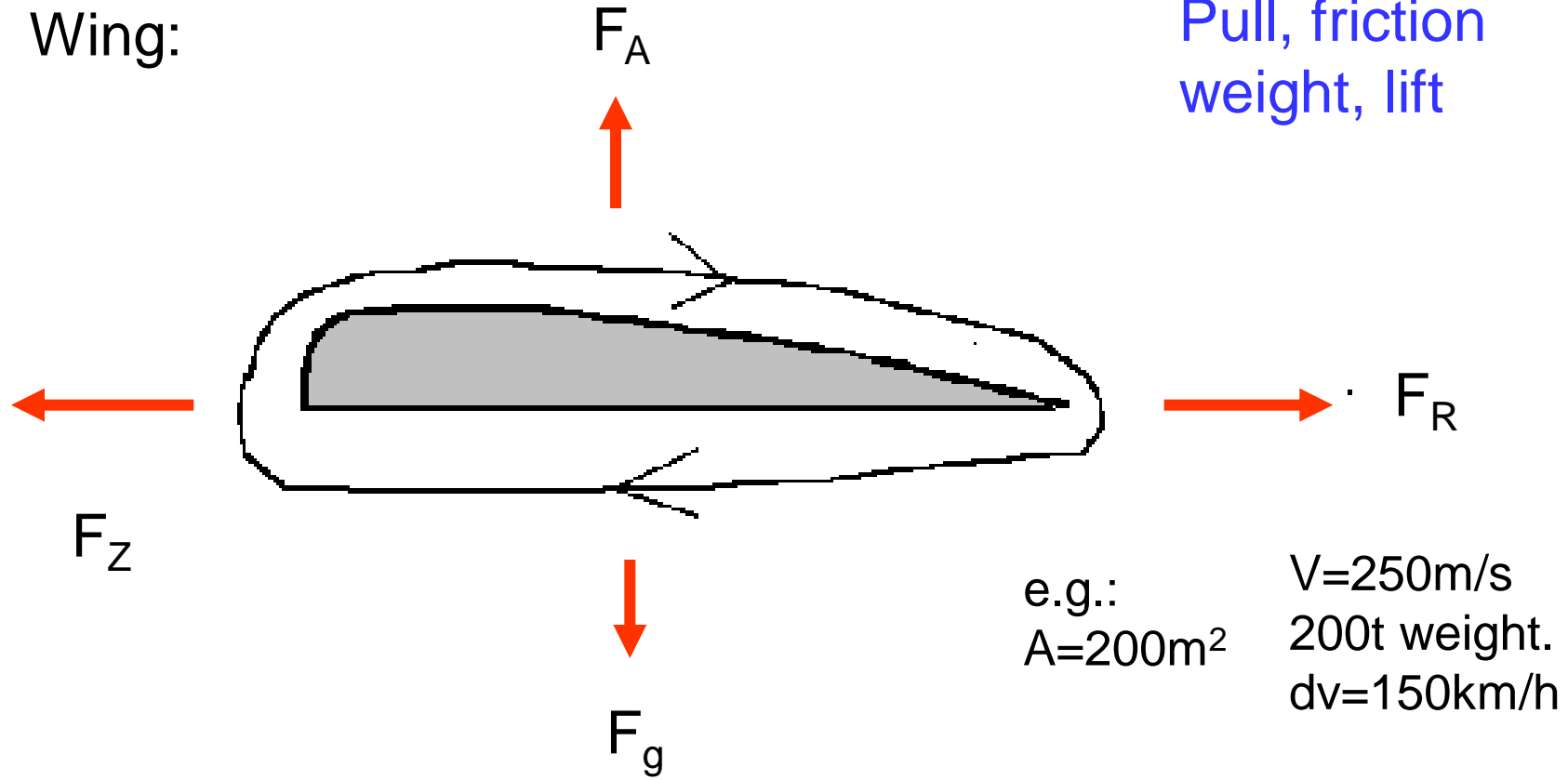
Tennis, table tennis, soccer etc.

Consequence:
Deflection

Rotating surface of the balls reduces/increases
via friction the velocity of air around the surface

Another example:

Wing:



Forces:
Pull, friction
weight, lift

e.g.:
 $A=200\text{m}^2$

$V=250\text{m/s}$
200t weight.
 $dv=150\text{km/h}$

$$F_A = A \cdot 0.5 \cdot \rho \cdot (v_{above}^2 - v_{below}^2)$$

$$F_A = A \cdot 0.5 \cdot \rho \cdot (v_{above} - v_{below}) \cdot (v_{above} + v_{below})$$

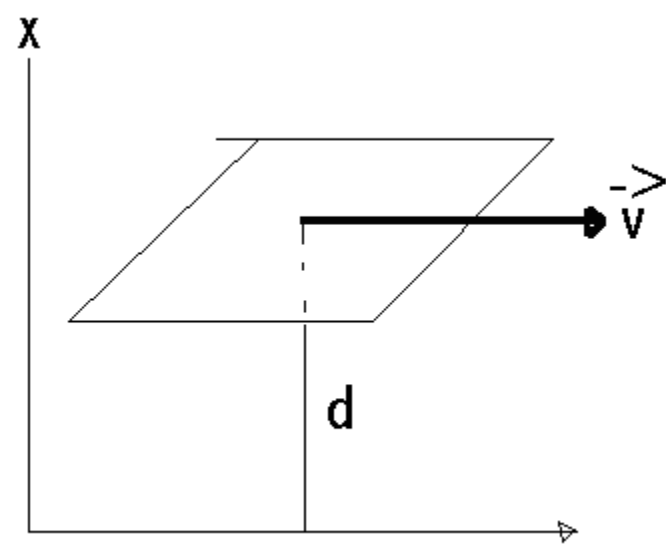
or with

$$(v_{above} + v_{below}) \simeq 2 \cdot v$$

Carrying force: $F_A \simeq A \cdot \rho \cdot v \cdot (v_{oben} - v_{unten})$

b) Laminary flow of viscous liquid

Liquid can **not** absorb **shear stress**.



Movable plate with surface S
In order to move a plate above a layer of liquid one needs a force:

$$F \sim S \cdot v/d$$

Interpretation: On a liquid act
a kind „shear tension“

$$\tau : \tau = F/S \quad d.h : \tau = \eta \cdot v/d \quad [\tau] = N \cdot m/S \quad \xrightarrow{\text{Viscosity}}$$

A sticking layer of liquid slides over the below lying layer etc.

v/d Stands for a velocity gradient $\rightarrow \frac{dv}{dx}$ e.g.: Gradient

$\eta(T) : T = \text{temperature, e.g. : } H_2O$

$$\eta(0) = 0.0018, \eta(100) = 0.00029$$

Example: **Laminary flux** between parallel plates, with $v = \text{constant}$

At surfaces: **Forces**

$$2 \cdot x \cdot b \cdot p_1 - 2 \cdot x \cdot b \cdot p_2$$

At wings: **friction forces:**

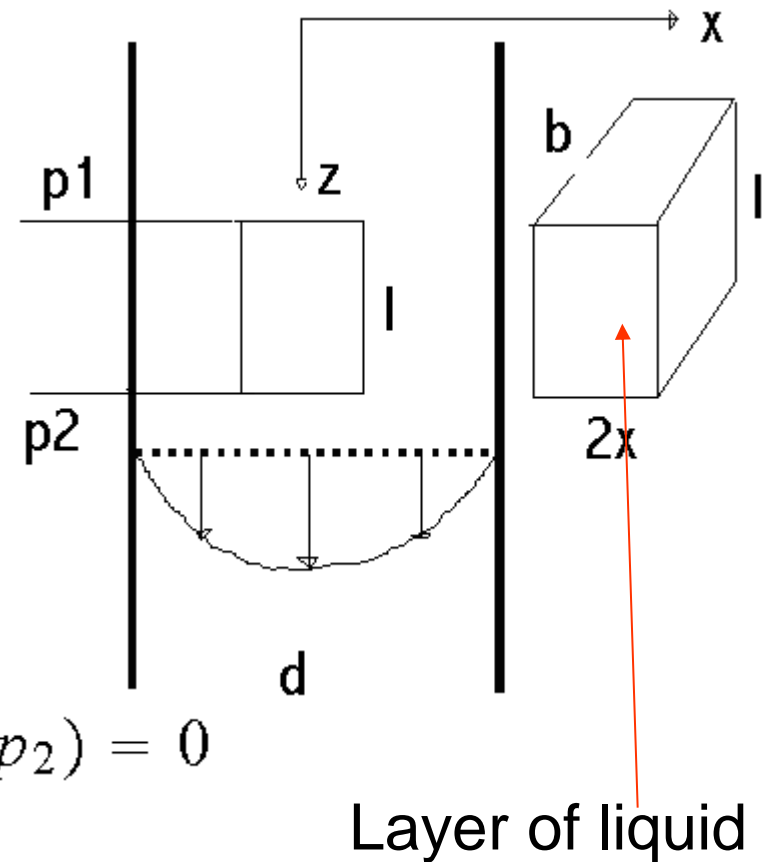
$$\eta \cdot 2 \cdot b \cdot l \cdot dv/dx$$

Constant velocity means:
The sum of all forces = 0!

$$\eta \cdot 2 \cdot b \cdot l \cdot dv/dx + 2 \cdot x \cdot b \cdot (p_1 - p_2) = 0$$

$$\rightarrow dv/dx = -x(p_1 - p_2)/(\eta \cdot l)$$

$$\text{Integration: } v = -x^2 \cdot (p_1 - p_2)/(2 \cdot \eta \cdot l) + c$$



$$v = -x^2 \cdot (p_1 - p_2)/(2 \cdot \eta \cdot l) + c$$

with $v=0$ for $x= d/2$
yields c to:

C integration constant

$$c = (d/2)^2 \cdot (p_1 - p_2)/(2 \cdot \eta \cdot l) \quad \text{and following:}$$

$$v = (p_1 - p_2)/(2 \cdot \eta \cdot l)((d/2)^2 - x^2) \quad (p_1 - p_2)/l = dp/dz$$

Stands for a gradient of pressure

$$\vec{v} \approx \text{grad}(p) \cdot ((d/2)^2 - x^2)$$

The tips of the vectors of velocity
lie on a parabola!

Laminary flux via a pipe can be dealt with
in analogy of the flat problem

$$r \cdot \eta \cdot 2 \cdot \pi \cdot l \cdot dv \cdot /dr + r^2 \cdot \pi \cdot (p_1 - p_2) = 0$$

$$dv/dr = -r \cdot (p_1 - p_2) / (\eta \cdot 2 \cdot l)$$

with integration:

$$-4 \cdot \eta \cdot l \cdot v / (p_1 - p_2) = r^2 + c$$

$$c = -R^2 \text{ für } v = 0 \text{ an } r = R$$

$$R^2 - r^2 = 4 \cdot \eta \cdot l \cdot v / (p_1 - p_2)$$

$$\text{or } v = (p_1 - p_2) \cdot (R^2 - r^2) / 4 \cdot \eta \cdot l$$

Paraboloid

Drifty mass of liquid for a time t:

$$dV = 2 \cdot \pi \cdot r \cdot dr \cdot v \cdot t = 2 \cdot \pi \cdot dr \cdot (p_1 - p_2) \cdot (R^2 - r^2) \cdot t / 4 \cdot \eta \cdot l$$

$$V = \frac{\pi \cdot (p_1 - p_2) \cdot t}{2 \cdot \eta \cdot l} \int_0^R (R^2 - r^2) \cdot r \cdot dr$$

$$V = \pi \cdot R^4 \cdot (p_1 - p_2) \cdot t / 8 \cdot \eta \cdot l$$

Flux:

$$\Phi = m/t = \rho \cdot V/t \rightarrow$$

Equation of Hagen- Poseuille

$$\Phi = \pi \cdot \rho \cdot R^4 \cdot (p_1 - p_2) / 8 \cdot \eta \cdot l$$

